

# Manganese Treatment and Distribution System Management

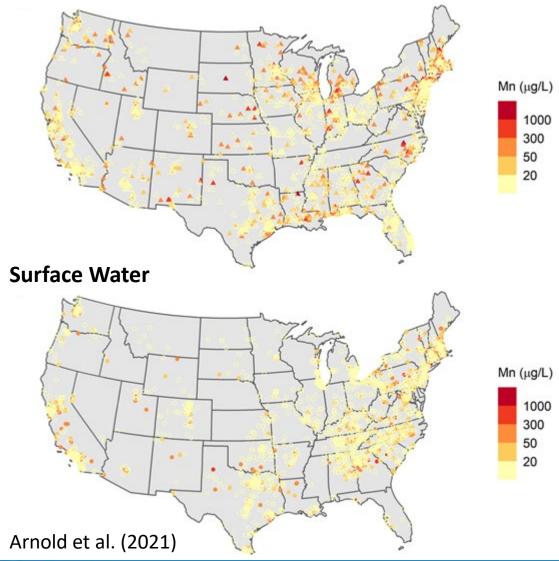
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## Mn Occurrence and Regulatory Status

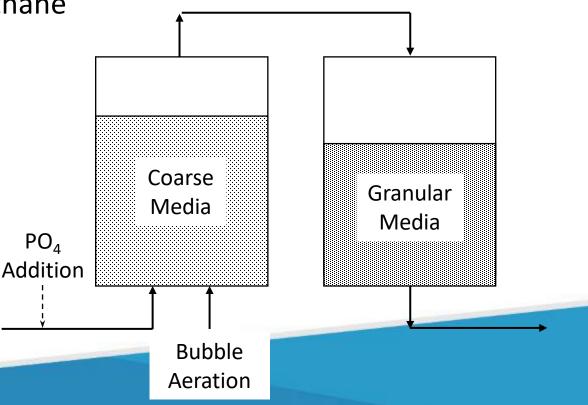
#### Groundwater



- Included in Unregulated Contaminant Monitoring Rule (UCMR) 4
  - Maps show maximum entry point concentration from UCMR 4 (2017-2021)
- Included on Contaminant Candidate List (CCL) 5
- Health Advisory Levels (HALs)
  - 0.3 mg/L for lifetime and infant acute
  - 1 mg/L for acute
- Secondary Maximum Contaminant Level (SMCL) = 0.05 mg/L

## Biological Treatment of Groundwaters

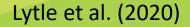
- Reducing conditions (low dissolved oxygen) with multiple contaminants
  - Ammonia, iron, arsenic, manganese, methane
- Aerated contactor + filter bioreactor
  - Continuous air sparging satisfies O<sub>2</sub> demand for nitrification ~ 4.6 mg O<sub>2</sub>/ mg NH<sub>3</sub>-N
  - Most oxidation occurs in contactor
  - Filter provides particle removal and additional oxidation

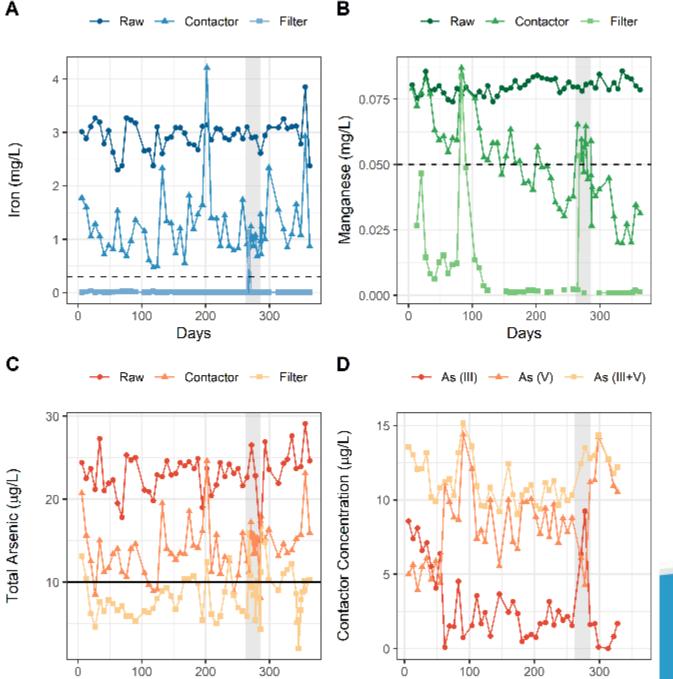


# Pilot- and Full-Scale <sup>·</sup> Small System in Iowa

• Pilot study August 2016 – July 2017

Parameter	Well		
Arsenic	27 μg/L		
Iron	4.25 mg/L		
Manganese	0.16 mg/L		
Ammonia	3.0 mg N/L		
тос	3.0 mg/L		
рН	7.55		
Hardness	$332 \text{ mg/L CaCO}_3$		
Alkalinity	410 mg/L CaCO $_3$		





Days

Days

# Pilot- and Full-Scale Treatment at a Small System in Iowa

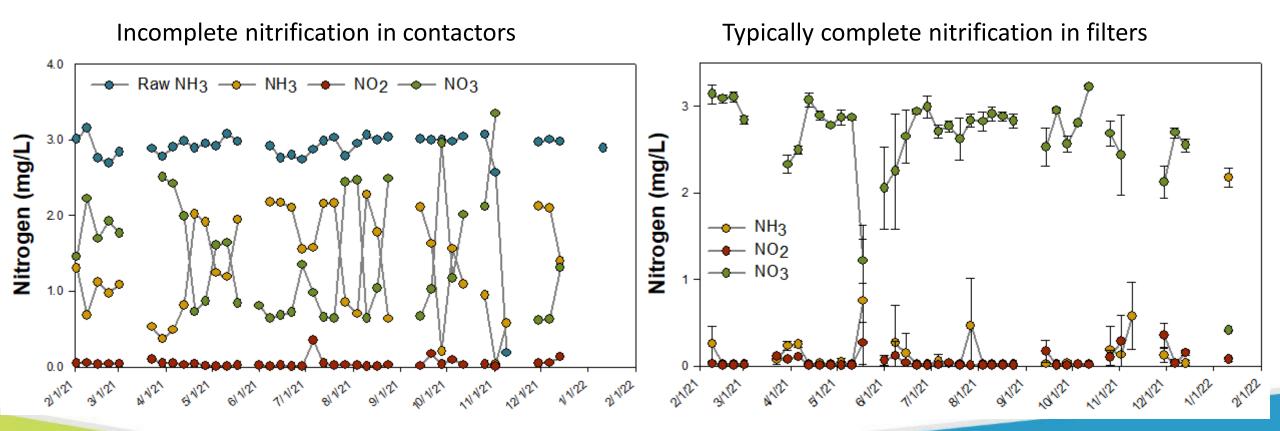
### **Full Scale Design**

Parameter	Units	Value	
Plant capacity	gpm	400	
Average day flow	gpm	180	
Number of contactors		2	
<b>Contactor diameter</b>	ft	11	
Contactor bed depth	ft	4.58	
Contactor media type		Gravel	
Contactor avg loading rate	gpm/ft <sup>2</sup>	0.95	
<b>Contactor avg EBCT</b>	min	36	
Number of filters		4 Anthracite/ Sand	
Filter media type			

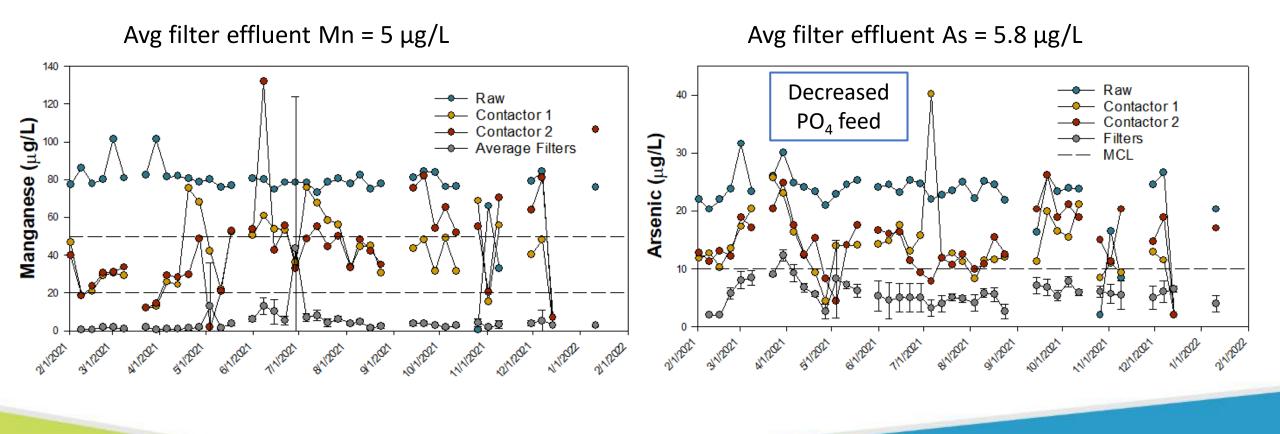
#### **Start Up Schedule**

Notes
Started flow through contactors
EPA-ORD sampling program started
Started flow through filters
Decreased PO <sub>4</sub> feed to improve arsenic removal
Online and operating at full capacity
EPA-ORD sampling program ended

# Pilot- and Full-Scale Treatment at a Small System in Iowa



# Pilot- and Full-Scale Treatment at a Small System in Iowa



**Key takeaway:** Aerated contactor + filter biotreatment system effectively treated arsenic, iron, manganese, and ammonia

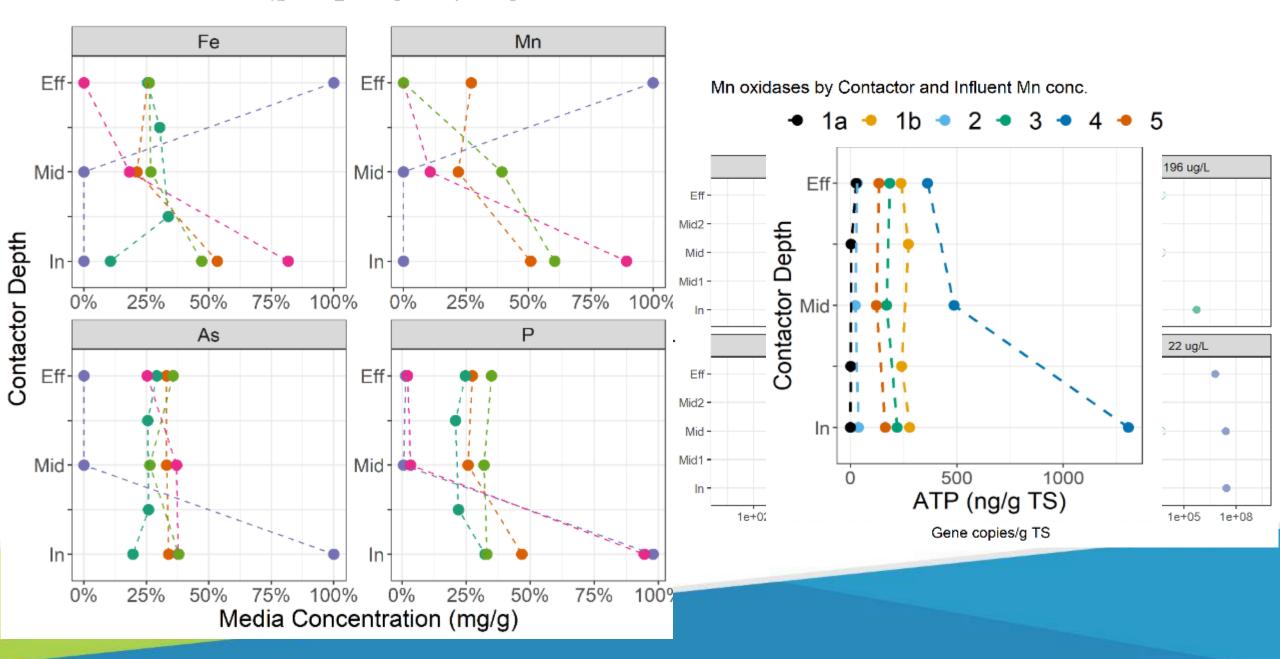
### Mn Removal within Aerated Contactor

- Where does Mn removal occur within aerated contactors?
  - Different mixing and DO profiles than filters
- What is the relationship between media surface Mn and Mn oxidases concentrations?
- Collected media samples at influent end, middle, and effluent end of 6 pilot-scale aerated contactors

Parameter	Range		
NH <sub>3</sub>	2.3 - 3.4 mg N/L		
Fe	0.1 - 3.95 mg/L		
Mn	2 - 196 µg/L		
As	< 4 - 23 μg/L		
тос	0.1 - 7.1 mg/L		
рН	6.5 - 7.9		
Hardness	ardness 215 - 374 mg/L CaCO <sub>3</sub>		

Parameter	Range	
Media Type	Ceramic, GAC, Gravel	
Loading Rate	3.1-7.3 m/h	
EBCT	9-25 min	
Air:Water Ratio	6-11 L/min:L/min	

🔸 1b 🔶 2 🔶 3 🔶 4 🔶 5



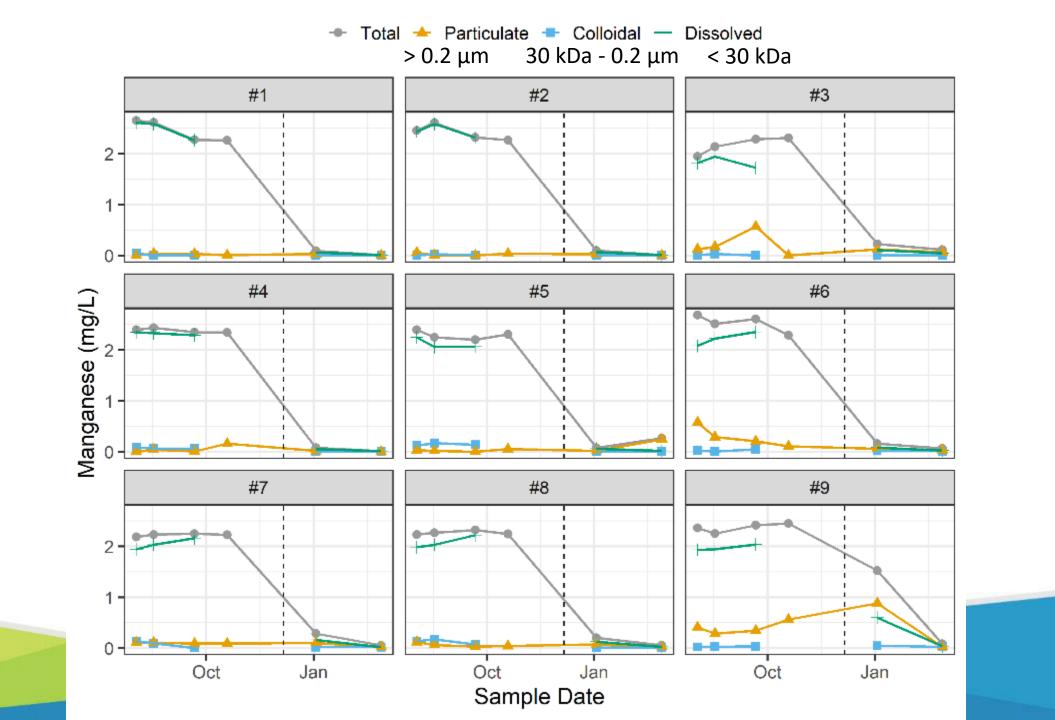
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## Distribution System Mn after Switching Sources

- System had been operating with Mn > 2 mg/L for decades
- Recently switched sources to a source with low Mn
  - Otherwise similar water quality
- Chloramines for disinfectant residual
- Dose blended PO<sub>4</sub>. Plan to slowly convert to ortho-PO<sub>4</sub> after system acclimates to new source
- Monthly sampling at entry point + 9 sites in the distribution system
  - 4 events before the switch
  - 3 events since the switch

## Water Quality – Entry Point

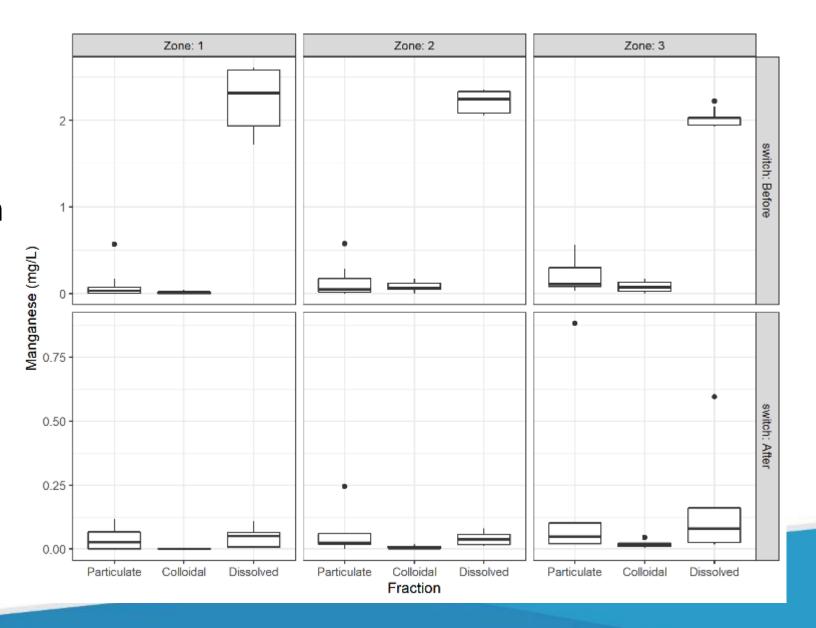
Parameter	Before Switch	After Switch	
рН	7.60	8.30	
Mn (mg/L)	2.29	0.021	
Fe (mg/L)	0.122	0.012	
Ca (mg/L)	72.7	55.7	
Mg (mg/L)	28.6	26.0	
Total Cl2 (mg/L)	1.30	2.29	



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## Mn Speciation

- Particulate > 0.2  $\mu$ m
- Colloidal 30 kDa-0.2  $\mu m$
- Dissolved < 30 kDa



### Summary

- Manganese is prevalent in regions throughout the U.S.
- A Mn regulation could necessitate systems to install treatment and manage legacy Mn in the distribution system
- Biological treatment of groundwaters with multiple contaminants via aerated contactor + filter consistently achieved Mn < 10  $\mu$ g/L
- Mn surface concentrations greatest at influent end of contactor and not related to Mn oxidases concentrations
- Total Mn decreased substantially after switching sources, but evidence of some instability in Mn particulates farther out in DS

#### Acknowledgements

- EPA: Matt Noerpel
- Water systems operators
- WesTech: Eric Lawrence, Tom Dumbaugh

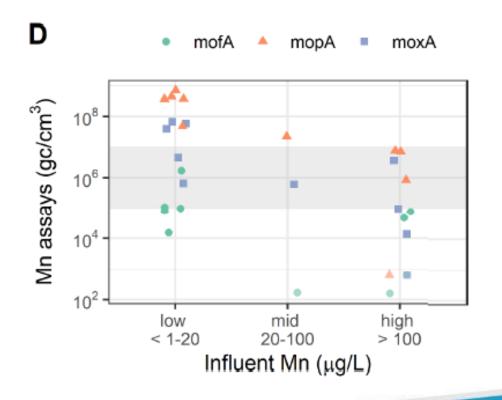
#### **Questions?**

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#### Notice

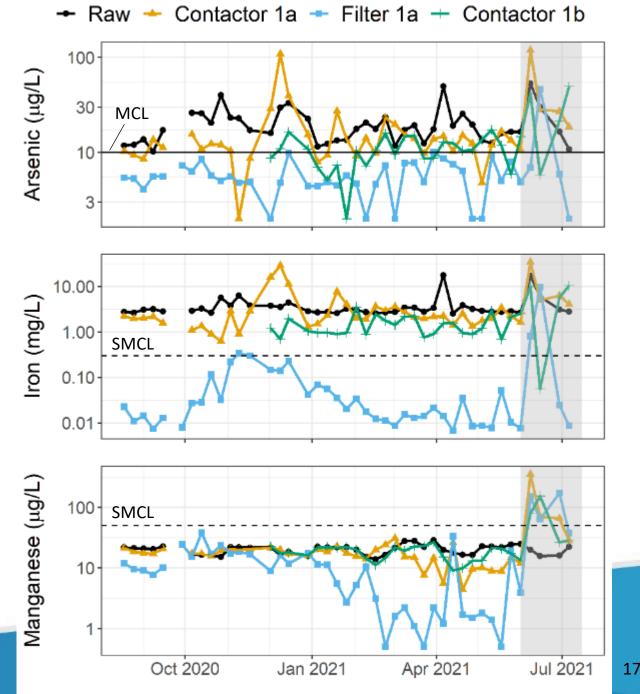
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- Apparent slight negative relationship between influent Mn concentration and Mn oxidases concentrations
  - Importance of abiotic removal mechanisms



# Site 1: Metals Removal

- Filter important for meeting treatment goals
- Arsenic
  - Oxidation + Fe particle removal
  - < MCL in filter effluent
  - 1-2-week acclimation time
- Iron
  - Oxidation + particle removal
  - 1-week acclimation time
- Manganese
  - Oxidation + surface coating
  - Improved in all 3 columns
  - 5-month acclimation time



## Additional Pilot Contactors for Comparisons

Contactor	Media	EBCT (min)	NH <sub>3</sub> [mg N/L] (% Removal)	Fe [mg/L] (% Removal)	Mn [µg/L] (% Removal)	As [µg/L] (% Removal)
1a	12 mm Gravel	9 ± 2	3.5 ± 0.4 (93%)	3.3 ± 0.9 (48%)	20 ± 4 (40%)	20 ± 9 (34%)
1b	2.2 mm Ceramic	16 ± 6	3.5 ± 0.4 (68%)	3.3 ± 0.9 (63%)	20 ± 4 (21%)	20 ± 9 (38%)
2	2.2 mm GAC	16	2.1 (59%)	3.1 (22%)	196 (53%)	< 2
3	2.0 mm Ceramic	16	3.1 (100%)	0.1 (23%)	57 (92%)	< 2
4	1.6 mm Ceramic	25	3.1 (100%)	1.1 (-41%)	52 (28%)	23 (-24%)
5	1.6 mm Ceramic	25	2.1 (85%)	2.1 (62%)	22 (-5%)	< 2

All systems dosed orthophosphate

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