Evaluation of Wood Chip Gasification to Produce
Reburn Fuel for Coal-fired Boilers

Robert E. Hall1,*, Chun Wai Lee1, Nick Hutson1, William Yelverton1 and Rolf E. Maurer2
*Corresponding author: hall.bob@epa.gov

1U.S. Environmental Protection Agency, Office of Research and Development, National Risk Management Research Laboratory, Air Pollution Prevention and Control Division (MD-E305-01), Research Triangle Park, NC 27711, USA
2Hamilton Maurer International, Inc., 12423 Broken Bough Drive, Houston, TX 77024, USA

Abstract: Gasification/reburning testing with biomass and other wastes is of interest to both the U.S. Environmental Protection Agency (EPA) and the Italian Ministry of the Environment & Territory (IMET). Gasification systems that use wastes as feedstock should provide a clean, efficient source of synthesis gas that has the combined benefit of producing energy or feedstock chemicals in an efficient manner while reducing the volume of wastes and minimizing their environmental impact, including reduction of oxides of nitrogen (NOx) and carbon dioxide (CO2). EPA has performed reburn tests with natural gas, oil, and pulverized coal in the past and both parties are interested in biomass and waste fuels due to the low cost of the fuel source and the impact on our landfills. EPA has a 4-MWth pilot-scale combustor that is capable of firing a variety of fuels. EPA will perform tests on this facility to evaluate the gasification of biomass to generate syngas for reburn to control NOx emissions while also displacing fossil fuels and reducing the associated CO2 emissions. With funding provided by IMET, Solar Heat and Power (SHAP) of Italy working with HMI, Inc. of the United States is designing a pilot-scale gasification unit and syngas line that will deliver raw syngas (biogas) to EPA’s combustor. The project will examine the feasibility of using syngas from gasification of wood as a reburn fuel that will use EPA’s Research Triangle Park (RTP) laboratory facilities to optimize gasification/reburn technology for reducing emissions from coal-fired industrial and utility boilers. The objective of this project is to demonstrate the feasibility of using wood chips as a feedstock (CO2 neutral) in a gasifier to provide a NOx reducing reburn fuel for coal-fired boilers. A NOx reduction of 50 to 65% or greater is anticipated in existing boilers.

Keywords: gasification, combustion, reburn, biomass, wood chips

1. INTRODUCTION

Biomass represents a large potential source of renewable energy with significant resource, economic, and environmental benefits. Advances in recovery of agricultural and forestry residues and industrial wastes, the production of dedicated energy crops, and the development of biomass conversion technologies improve the competitiveness of biomass energy over conventional fossil energy. Also, biomass energy can provide major environmental benefits compared with fossil energy use with regard to emissions of pollutants and greenhouse gases in particular. The cost of waste disposal has increased recently due to a combination of environmental concerns in conjunction with the availability and cost of landfills. The use of biomass waste materials as the feedstock in a gasification process becomes increasingly attractive for its potential of eliminating the waste disposal costs while producing clean and renewable energy [1]. A wide range of biomass such as agricultural and forest residues and industrial wastes from pulp and paper and furniture industries are potential readily available biomass gasification feedstock. Biomass gasification is highly versatile with widely different process designs such as fixed- and fluidized-beds, air- and oxygen-blown, and product gases including low and medium Btu gases for adapting to different feedstock and end use requirements [1].

Gasification and reburning testing with biomass waste fuel is of interest to both the EPA and IMET. EPA has performed reburning tests with natural gas, oil, and pulverized coal in the past and both parties are interested in biomass fuels due to the low cost and renewable properties of the fuel source. The Air Pollution Prevention and Control Division (APPCD) of EPA has a pilot-scale combustor that is capable of firing a variety of fuels. APPCD will perform tests on this facility to evaluate the gasification of biomass for reburning to control nitrogen oxides (NOx) emissions. IMET will design, fabricate, and install a pilot scale gasification unit and syngas delivery system that will connect to APPCD’s combustion facility. The gasification and reburning project will examine the feasibility of using syngas from gasification of waste, in this case wood chips, as a reburning fuel. The project will use the EPA’s facilities to maximize the environmental benefits of gasification/reburning technology for reducing emissions from coal-fired industrial and utility boilers. The objective of this project is to demonstrate the use of biomass in a gasifier to produce a reburning fuel for coal-fired boilers to reduce their NOx emissions. A 50% to 65% NOx reduction is anticipated in existing coal-fired boilers.

2. BIOMASS GASIFICATION REBURNING PROJECT

2.1 Reburning for NOx Emissions Control
Reburning is a combustion modification technology that removes NOx from combustion products by using fuel as a
reducing agent. To implement the reburning process in a combustor, the combustion air and fuel are divided into three zones that stage the fuel and air addition to the furnace. In the primary combustion zone, the main fuel is burned under normal fuel-lean conditions to release about 80% of the total heat input to the furnace. The reburning fuel, which accounts for the other 20% of the fuel input, is injected into the reburning zone that is located downstream of the primary zone to form a slightly fuel-rich zone where NO\(_x\) from the primary zone is reduced. The hydrocarbon free radicals generated from breakdown of the reburning fuel under fuel-rich conditions react with NO\(_x\) to form molecular nitrogen (N\(_2\)) and water in the reburning zone. Additional combustion air is added in the final burnout zone to oxidize CO and any remaining fuel under overall fuel-lean conditions. In addition to syngas (CO and H\(_2\)), significant quantities of tar and oil are produced from the biomass gasification process. These liquids (aerosol) tend to breakdown into smaller hydrocarbon fragments in the combustion process. The potential for using these liquids as a reburning fuel for producing reactive hydrocarbon free radicals for effective NO\(_x\) reduction will be evaluated in the joint EPA/IMET reburning study.

2.2 EPA Combustion Research Facility

A biogas reburning system will be added to APPCD’s existing Multi-pollutant Control Research Facility (MPCRF) to study gasification of biomass for reburning to control NO\(_x\) emissions. The MPCRF, shown in Figure 1, is a state-of-the-art facility that can be used to examine the formation and control of nitrogen oxides (NO\(_x\)), sulfur dioxide (SO\(_2\)), mercury (Hg) and other heavy metals in coal-fired boilers. The MPCRF is located in the High Bay of EPA’s Research Triangle Park, NC campus and its combustor (4 MMBtu/hr) can be operated on natural gas, fuel oil, or pulverized coal. The MPCRF is currently equipped with a low NO\(_x\) burner; electrostatic fabric filters (ESFF), electrostatic precipitator (ESP), and a wet scrubber. A selective catalytic reduction (SCR) unit is also used for deep NO\(_x\) control, and the electrostatic precipitator (ESP) was added recently as an alternative for particulate matter (PM) control. The MPCRF’s unique design enables it to perform parametric studies on the controls of multiple pollutants under a variety of conditions. The facility is equipped with continuous emissions monitors (CEMs) for measuring carbon dioxide (CO\(_2\)), carbon monoxide (CO), oxygen (O\(_2\)), SO\(_2\) and NO\(_x\). State-of-the-art mercury CEMs are also installed for collecting real-time results on Hg control tests under a variety of test conditions.

Fig. 1 Schematic of MPCRF
2.3 CFD Modeling Study
The technical feasibility of adding a reburning system to the MPCRF furnace will be evaluated by conducting a computational fluid dynamic (CFD) modeling study of the MPCRF’s existing coal combustion furnace. The objectives of the study are to analyze the flow and temperature patterns in the furnace burning an Eastern bituminous coal, and to identify the optimum locations for injecting the syngas products as the reburning fuel to reduce NO\textsubscript{x} emissions produced by the pilot-scale gasification unit that will be co-located with the MPCRF. The furnace section is 20 ft in height and 3.5 ft in inner diameter, with a swirl burner installed at the top of the furnace. The burner is patterned after the original movable block swirl burner developed by the International Flame Research Foundation. The furnace is designed to generate 1,000 SCFM flue gas at full firing rate. The reburning system is required to contribute 20% of the total heat input to the MPCRF furnace (at 4 MMBtu full firing rate) with up to 65% or greater NO\textsubscript{x} reduction.

2.4 Biomass Gasifier Design
Working with Hamilton Maurer International (HMI) of the U.S., Solar Heat and Power (SHAP) of Italy is providing the design of a pilot-scale downdraft dry-ash, single-stage, fixed bed gasifier for the reburning project. The design work, initiated in mid-2008, was completed in late-2008. Biomass fuels are generally more reactive and have higher moisture content than coal. The raw gas conversion efficiency of the single-stage fixed-bed gasifier [2] is in the range of 80 to 90 percent of the energy feed being delivered to the reburning zone as gas and pyrolysis liquids depending on the moisture content of the fuel. The syngas is expected to result in a significant NO\textsubscript{x} reduction in the reburning zone and the intent of the research is to establish the operational requirements to optimize (maximize) the NO\textsubscript{x} reduction.

The composition of the syngas, which is delivered to the reburning zone, will be continuously monitored by using CEMs. An Electrostatic Gas Cleaning System (EGCS) designed and supplied by HMI will be used to remove tar and moisture from the sampled raw gasification products to produce a clean gas sample for the CEM measurements. The EGCS first cools the raw gas sample to nominally 100 °F to insure that all pyrolysis liquids (tars) are condensed within the gas sample (10 L/min sample flow). The tar droplets (aerosol) are completely removed (99.99%) from the sampled gas using electrostatics by the EGCS based on HMI’s demonstrated wet electrostatic precipitator design [2]. The gas is further dried and filtered prior to delivery to the CEMs. The tar/water mixture removed by the EGCS is collected and the water separated from the tar prior to preparing the tar sample for ultimate analysis. The analysis will provide heating value and the elemental composition of the oil/tar component of the biogas, which will be used for calculating the mass and energy balance of the gasification process and the detailed composition of the reburn fuel. The tar fog created by the gasifier and injected into the combustor is important because it is expected to significantly enhance the NO\textsubscript{x} reduction via the tar’s high reactivity within the reburning zone as demonstrated by early biogas reburn work performed for ENEL in Italy by Ansaldo Ricerche which motivated this IMET-U.S. EPA collaboration. Those bench-scale tests resulted in a NO\textsubscript{x} reduction of 70% or greater.

The reburning process is designed to be operated at a nominal 20% heat input provided by the reburning fuel produced from gasification of biomass. The energy fraction of the tars contained within the raw product gas will be included in the total energy delivered with the syngas to the reburning zone. The tar content (fraction in the raw product gas) and the tar composition will be biofuel specific. It is anticipated that the tar content in the raw product gases will range from a high of 30% to a low of 10%. The biomass gasification unit is designed to be operated at a nominal rate of 140 to 170 lb/hr of biowaste fuels with a heating value in the range of 4,000 to 7,000 Btu/lb to deliver nominally 0.8 MMBtu/hr heat input required by the reburning process in the MPCRF furnace.

A key aspect of this project will be the continuous monitoring of the gaseous and liquid products generated within the gasifier and delivered to the reburning zone of the boiler to meet the 0.8 MMBtu/hr reburning fuel input. The gasification unit will be operated to deliver syngas and liquids (oil and tar) at a total flow rate in the range of 60 to 90 standard cubic ft per minute (scfm) for injecting into the reburning zone of the MPCRF furnace to achieve the 0.8 MMBtu/hr nominal energy input for NO\textsubscript{x} reduction. The typical design output of the gasification unit is listed in Table 1. The dry syngas produced by the gasification of a biofuel (wood) contains 16.8% CO, 13.7% H\textsubscript{2}, 11.5% CO\textsubscript{2}, and 56.5% N\textsubscript{2}, 0.8% O\textsubscript{2}, and trace hydrocarbons (CH\textsubscript{2}CH\textsubscript{2}, C\textsubscript{2}H\textsubscript{4}) with a higher heating value (HHV) of 122 Btu/scf. The pyrolysis liquids will contribute up to 30% of the energy to the reburning zone. The tar fog has a droplet mass mean diameter of 2.6 micron\textsuperscript{2}. The small tar droplets with high surface area are highly reactive to provide effective NO\textsubscript{x} reduction in the reburning zone of the boiler. The fabrication and installation of the gasifier at RTP is expected to occur in late-2008. Testing with gasification of wood chips is scheduled to begin in 2009. Initial tests will be run with the combustor firing natural gas followed by tests with pulverized coal. Additional tests may be performed with gasification of other waste materials depending on the outcome of the initial tests and future funding.
Table 1 Summary of Typical Output of the Biomass Gasifier

<table>
<thead>
<tr>
<th>Output</th>
<th>lb/hr</th>
<th>MMBtu/hr</th>
</tr>
</thead>
<tbody>
<tr>
<td>Dry Gas</td>
<td>222</td>
<td>0.539</td>
</tr>
<tr>
<td>Water in Gas</td>
<td>121</td>
<td>0.129</td>
</tr>
<tr>
<td>Oil and Tar</td>
<td>18</td>
<td>0.323</td>
</tr>
<tr>
<td>Bottom Ash</td>
<td>2</td>
<td>0.0</td>
</tr>
<tr>
<td>Fly Ash</td>
<td>1</td>
<td>0.009</td>
</tr>
<tr>
<td>Total</td>
<td>364</td>
<td>1.0</td>
</tr>
</tbody>
</table>

3. REFERENCES
