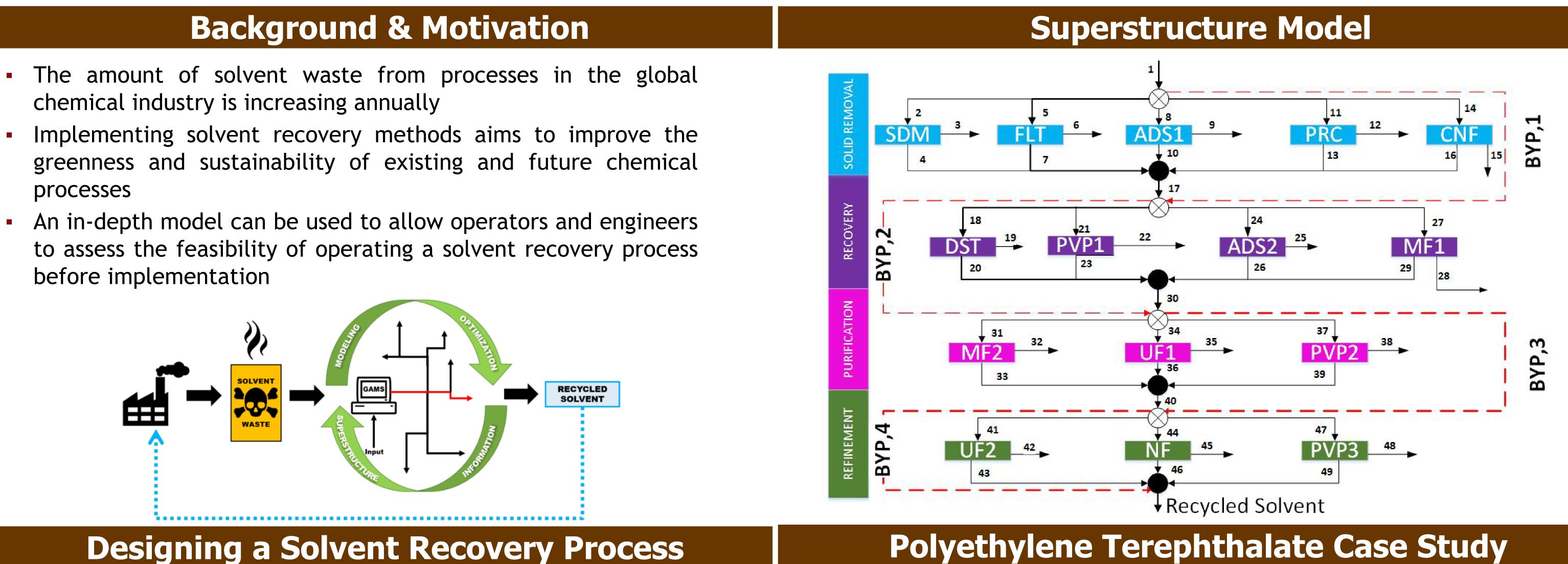
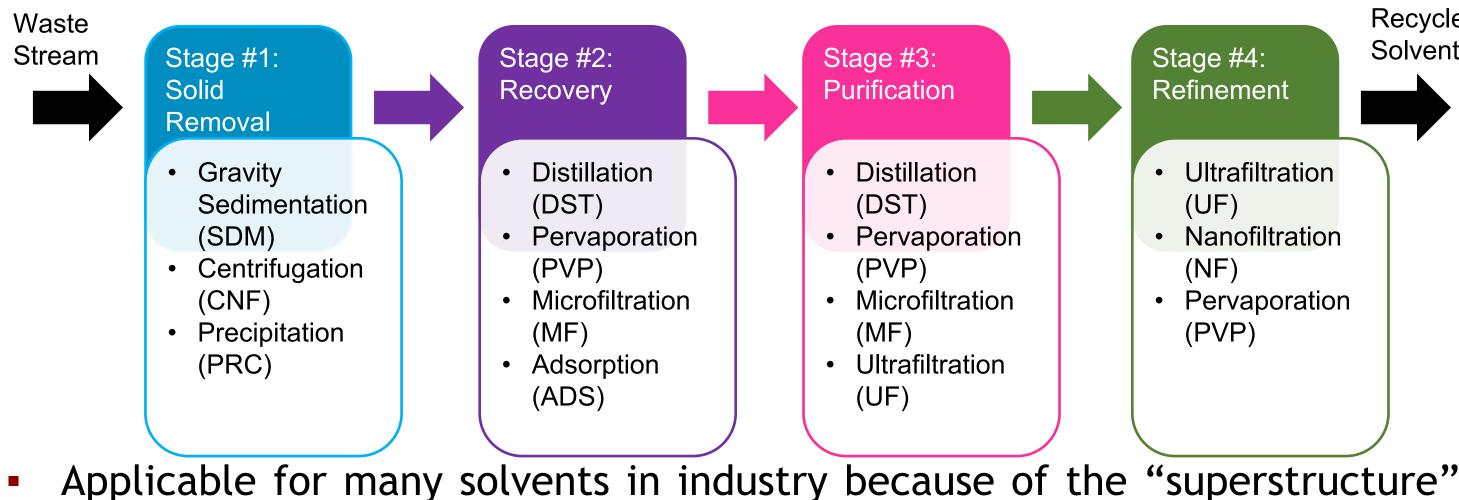
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- chemical industry is increasing annually
- processes
- before implementation





- approach, which provides simultaneous comparison of all possible options to reach the desired result
- Additional stages of separation are implemented based on purity requirements

Technology Models

Model Statistics

Statistic	Value
Number of equations	657
Number of variables	435
Discrete Variables	19
Solution Time (s)	0.375

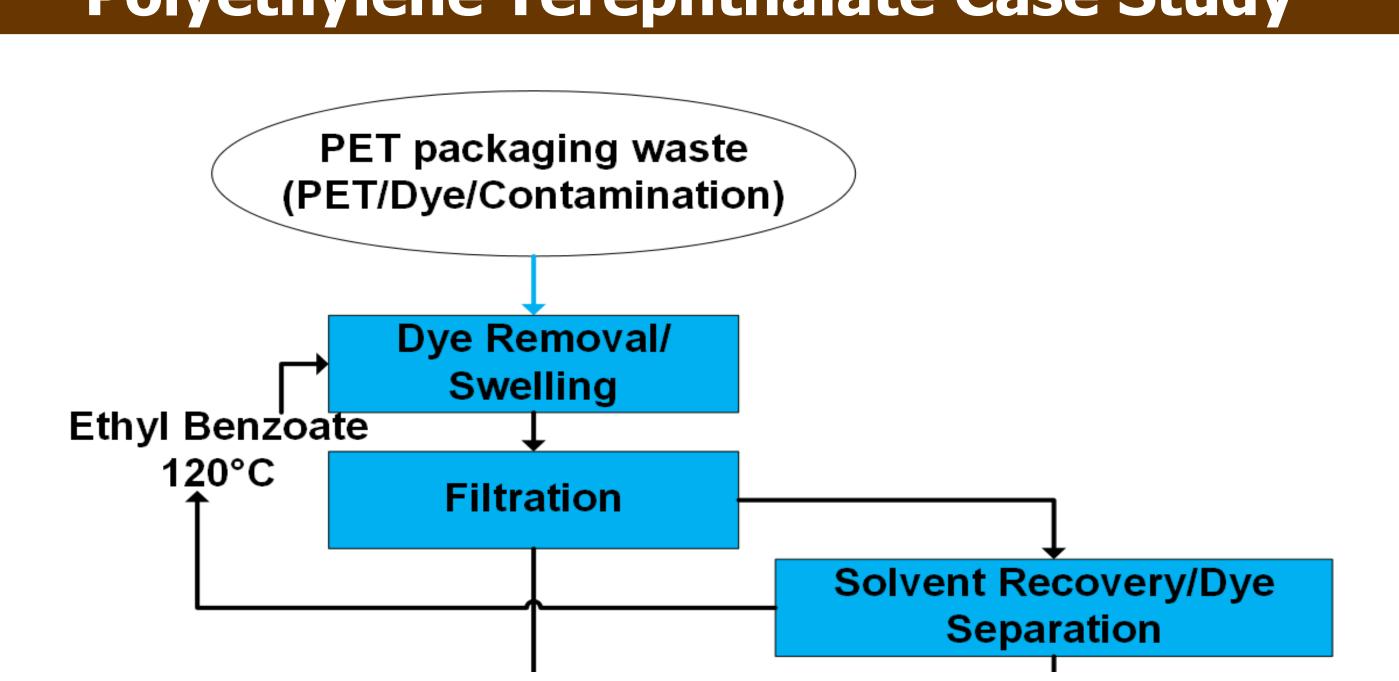
$$\boldsymbol{\xi_{k,UF}} = \frac{M_J}{M_{JI}}$$

$$CF_{UF} = \frac{\sum_{k \in K_{j}, Jfeed_{UF}} \left(\frac{M_{j,k}}{\rho_{k}}\right)}{\sum_{k \in K_{j}, Jretentate_{UF}} \left(\frac{M_{j,k}}{\rho_{k}}\right)}$$

$$\zeta_{UF} Q_{C_{UF}} = \sum_{\substack{k \in K_j \\ j \in J_{feed_{UF}}}} \left(\frac{M_{j,k}}{\rho_k}\right) \left(1 - \frac{1}{CF_{UF}}\right)$$

Superstructure Design of Solvent-Assisted Plastics Recycling Processes

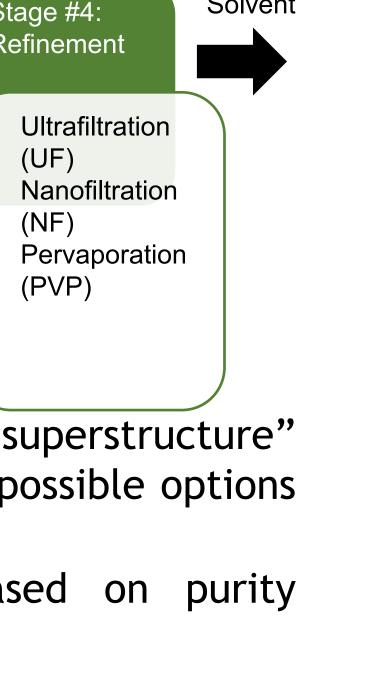
Brandon Jarrett¹, M. Mackley¹, L. Clarke¹, J. P. Stengel¹, A. L. Lehr¹, E. A. Aboagye¹, G. J. Ruiz-Mercado², J. F. Stanzione¹ and K. M. Yenkie¹ ¹Chemical Engineering, Henry M. Rowan College of Engineering, Rowan University, NJ - 08028, USA ²Office of Research & Development, U.S. Environmental Protection Agency, Cincinnati, OH, 45268, USA Disclaimer: The views expressed in this poster are those of the authors and do not represent the views or policies of the U.S. EPA



- Analyzing a case study involving the recycling of Polyethylene Terephthalate (PET) using solvent ethyl benzoate
- Producing results using this case study for input specifications provides proof of concept of the tool
- Shows the broad impact of the implementation of solvent recovery across multiple industries.

Chemical	Mass (kg/hr)	Inlet Mass Fraction	Output Requirements
PET	100	0.0421	Removal: >95%
Ethyl Benzoate	2278	0.9575	Purity: >99%
Additives	0.5	0.0002	Removal: >95%
Acetaldehyde	0.5	0.0002	Removal: >95%

- Inlet and outlet specifications are determined Purity or recovery is specified for desired solvents and removal is specified for undesired chemicals



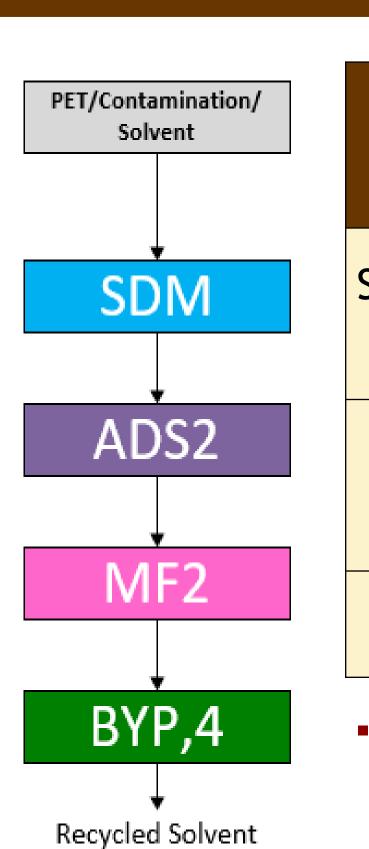
Recycled

Solvent

Model Equations (Ultrafiltration)

 $\frac{Jr_{UF'k}}{K}$; $\forall k \in K_i$ Jin_{UF},k

 $PW_{UF} = Wsp_{UF}Qc_{UF}$



Stage	Annualiz Cost (\$/
SDM	932
ADS2	527
MF2	393,53
BYP, 4	0

- optimal pathway

Summary and Future Work

- with industrial solvent waste
- superstructure model
- superstructure model

Acknowledgements

- This work is sup Agency's Pollu (NP96259218)

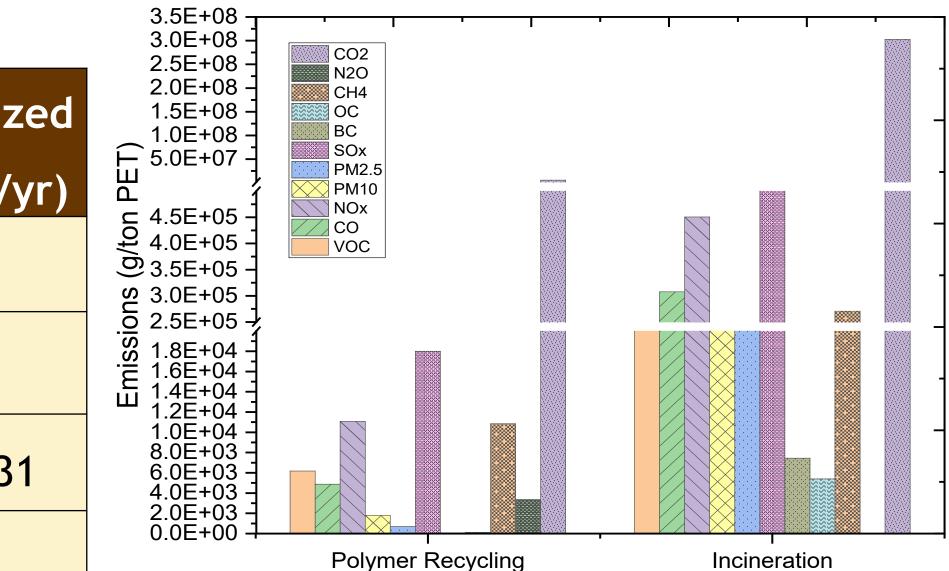
Contact Information



PET Case Study Results

Recovery Pathways	Annualized Cost (\$ million/yr)	Prices (\$/kg processed)
SDM-ADS2-MF2- BYP4	0.394	0.02
ADS1-ADS2- MF2-BYP4	0.431	0.03
Incineration	7.72	0.43

12.25 metric tons ethyl benzoate/yr (99%) Purity).



Handling Method

Cost per stage along with environmental impact of the most

Incineration produces magnitudes more emissions and costs nearly 20 times more than solvent recovery

Superstructure model provides alternative methods to dealing

Perform addition case studies to further develop the

Continue to add more seperation technologies into the

Rowan University Chemical Engineering Department

Sustainable Design and Systems Medicine Lab

pported	by the U.S.	Environ	mental	Protection
ution	Prevention	(P2)	Grant	Program

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