# Nitrous Oxide Emissions From Fossil Fuel Combustion

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The role of coal combustion as a significant global source of nitrous oxide (N<sub>2</sub>O) emissions was reexamined through on-line emission measurements from six pulverized-coal-fired utility boilers and from laboratory and pilot-scale combustors. The full-scale utility boilers yielded direct N<sub>2</sub>O emission levels of less than 5 ppm. The sub-scale combustor test data were consistent with full-scale data, and also showed N<sub>2</sub>O emission levels not exceeding 5 ppm, although these levels increased slightly when various combustion modifications to lower NO emissions were employed. These on-line emission measurements are very different from previously published data. The discrepancy is shown to be due to a sampling artifact by which significant quantities of N<sub>2</sub>O can be produced in sample containers which have been used in establishing the previously employed N<sub>2</sub>O data base. Consequently, we conclude that N<sub>2</sub>O emissions bear no direct relationship to NO emissions from these combustion sources, and that this direct source of N<sub>2</sub>O is negligible. Other indirect routes for the conversion of NO into N<sub>2</sub>O outside the combustor and other combustion sources not examined by this study, however, cannot be ruled out.

#### INTRODUCTION

The atmospheric concentration of nitrous oxide (N<sub>2</sub>O) is reported to be increasing at a rate of between 0.18 and 0.26 percent per year [Weiss, 1981; Khalil and Rasmussen, 1983]. This is a matter of concern because N2O has been implicated as both a "greenhouse" gas and a reactant in stratospheric ozone depletion mechanisms. Fossil fuel combustion has been proposed as being the major contributor to the measured increases in ambient N2O concentrations, as these increases seem to track measured increases in ambient CO2 concentrations. Furthermore, Hao et al. [1987] presented data of direct N2O emissions from fossil fuel combustion, indicating stack emissions exceeding 100 ppm N2O, and an approximate average N<sub>2</sub>O-N:NO<sub>x</sub> molar ratio of 0.58:1. From these data, Hao et al. confirmed earlier suggestions [Pierotti and Rasmussen, 1976; Weiss and Craig, 1976] that combustion of fossil fuels represents a dominant factor in the observed increase of N2O and that, consequently, combustion related sources of N2O increased rapidly during the twentieth century, in parallel with the volume of coal being burned. Using their N2O/NO, emission ratio and future projections of coal usage, these authors were then able to project a 20 percent increase in atmospheric N2O concentrations by the year 2050. This corresponds to a 367 ppb atmospheric concentration by the year 2050 from its 1987 level of

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Paper number 89JD03579. 0148-0227/90/89JD-03579\$05.00 approximately 303 ppb. They also suggested that deployment of low  $NO_x$  burners may offer a means to reduce anthropogenic emissions of  $N_2O$  in the future.

The N2O emissions from fossil fuel combustion reported by Hao et al. [1987] can be put into perspective through an analysis of the anthropogenic N2O flux. Weiss [1986] estimates the total anthropogenic N2O flux to be approximately 1.4 x 1011 g-moles/yr (approximately 32 percent of the total flux). World energy usage (global market) in 1975 was estimated to be approximately 223.5 Quads (2.235 x 10<sup>17</sup> Btu) [Kavanaugh, 1986]. By assuming that the fraction of the world energy derived from coal combustion is the same as that for the U.S. (approximately 21 percent) [Kavanaugh, 1986], and assuming the volumetric air requirements of a medium value bituminous coal and 20 percent excess air, then the necessary concentration of N2O in the exhaust gases of all coal combustion sources to account for the entire anthropogenic flux is approximately 175 ppm. Comparison of this figure with the 100 ppm N<sub>2</sub>O emission levels measured by Hao et al. [1987], strongly suggested coal combustion to be a dominant source of the global anthropogenic N2O flux.

The argument that coal combustion might be a significant source of global N<sub>2</sub>O emissions was further strengthened by the fundamental work of *Kramlich et al.* [1989], who showed that fuel nitrogen release from fossil fuels in the cooler portion of a combustor could result in significant quantities of N<sub>2</sub>O in the exhaust gas. *Martin and Brown* [1987] reported similar N<sub>2</sub>O increases at the quenched edges of laminar flames. Whether the appropriate conditions actually occur in full-scale coal combustors was not determined. Fundamental

considerations, however, did not support the suggestion that a constant N<sub>2</sub>O/NO<sub>x</sub> molar ratio was applicable for coal combustion sources in general. The U.S. Environmental Protection Agency (EPA) initiated a research program to stimulate collaborative national and international research programs with industry, academia, and other government agencies to better characterize and understand the anthropogenic sources of N<sub>2</sub>O. Partial results from these programs, which have been reported in the proceedings of three workshops sponsored by EPA [Lanier and Robinson, 1986; Kramlich et al., 1988; Ryan and Srivastava, 1989], suggested the need to undertake additional combustion research to substantiate the N<sub>2</sub>O emission data base on which so many of the previous conclusions relied. Results from portions of this investigation are presented here.

The present paper is concerned solely with a re-examination of the issues relating to the direct role of combustion sources on the observed global rise of N2O in the atmosphere. Other anthropogenic sources or natural sources [Cofer et al., 1988; Anderson et al., 1988; Levine et al., 1988] of N2O are not discussed. Specifically, we address the following issues: how valid is the historical N2O data base; how valid is the use of the N2O/NOx emission ratio, reported above; to what extent can apparent discrepancies between different sources of data be explained through a sampling artifact; and what is the potential impact of NO<sub>x</sub> abatement procedures on N<sub>2</sub>O emissions from combustion sources? These questions are addressed through the application of on-line N2O measurement techniques to extracted flue gas samples from several full-scale pulverized-coal-fired utility boilers and from laboratory combustors burning pulverized coal, fuel oils, and natural gas. Furthermore, discrepancies between the on-line N2O measurements and those constituting the historical data base are then examined in detail, and the relationship of these discrepancies to a sampling artifact which influenced the existing data base is explored. Results allow a reassessment of

the role of direct coal combustion N<sub>2</sub>O emissions in the global N<sub>2</sub>O budget. However, since secondary reactions converting NO to N<sub>2</sub>O in the sample containers were found to occur at room temperature [Muzio and Kramlich, 1988; de Soete, 1988; Muzio et al., 1989; Lyon and Cole, 1989; Lyon et al., 1989], an indirect relationship between NO emissions and the global N<sub>2</sub>O increase cannot be ruled out at this time, without further research in atmospheric conversion chemistry.

### . HISTORICAL DATA BASE

A summary of the N<sub>2</sub>O data base from stationary fossil fuel combustion as presented by Hao et al. [1987] is presented in Figure 1. The open symbols represent data reported by that group from three studies [Castaldini et al., 1982]. Shaded symbols represent preliminary on-line measurements taken by our group, using a laboratory-scale downfired coal combustor (2.3 kg/hr, 5 lb/hr) burning two western coals. Also included in Figure 1 is a line representing the proposed N<sub>2</sub>O-N:NO<sub>x</sub> molar ratio of 0.58:1 [Hao et al., 1987]. Clearly, the significant discrepancies between these data sets cast doubt both on an N<sub>2</sub>O emission factor that was proportional to NO<sub>x</sub> emissions from fossil fuel combustors, and on its use to estimate the global flux of N<sub>2</sub>O resulting from this source.

Additional data gathered by a number of research groups using various on-line and container sampling methods served only to increase the scatter. An explanation for this scatter was presented at the third N<sub>2</sub>O workshop (June 1988) [Ryan and Srivastava, 1989], when data presented by one research group suggested the presence of an N<sub>2</sub>O sampling artifact [Muzio and Kramlich, 1988]. They presented evidence that indicated that N<sub>2</sub>O might be produced in sampling containers awaiting analysis. They further hypothesized a mechanism of this formation involving NO, SO<sub>2</sub>, and water. This evidence questioned the validity of all existing data which involved container sampling.

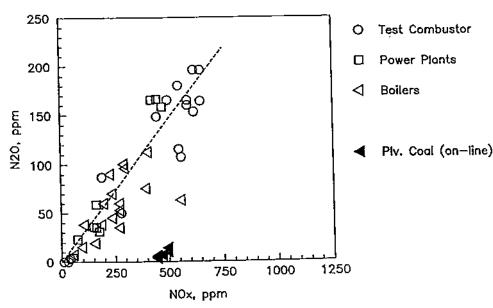


Fig. 1. Historical N2O/NO<sub>X</sub> data base. Open symbols represent the data presented by Hao et al. [1987]. Shaded symbols represent preliminary data taken by this group burning two western coals in a laboratory-scale combustor using an on-line GC/ECD sampling/analysis technique. The dashed line represents a proposed N2O-N:NO<sub>X</sub> molar ratio of 0.58:1 [Hao et al., 1987].

As a consequence of these new developments the EPA, through its Air and Energy Engineering Research Laboratory (AEERL), renewed efforts to characterize, by on-line means, direct N<sub>2</sub>O emissions from several laboratory and pilot-scale combustion systems burning a variety of coals, fuel oils, and natural gas. Additionally, we sought to compare the results from these sub-scale systems to direct N<sub>2</sub>O measurements (by on-line techniques) from full-scale pulverized-coal-fired utility boilers. Furthermore, in order to reconcile the apparent discrepancies between old and new data in terms of the sampling artifact reported by Muzio and Kramlich [1988], we also characterized the time dependent evolution of N<sub>2</sub>O, NO, and SO<sub>2</sub> in container samples of various moisture contents.

#### On-LINE MEASUREMENTS

## Laboratory and Pilot-Scale Experiments

Three EPA combustion systems that were used for the subscale experiments included a 29 kW (100,000 Btu/hr) refractory-lined, downfired, coal-fired tunnel combustor (Downfired Tunnel Furnace), a 733 kW (2,500,000 Btu/hr) gas/oil-fired, firetube package boiler (North American Boiler), and an 588 kW (2,000,000 Btu/hr) gas/oil-fired, watertube package boiler simulator equipped with a precombustion-chamber low NO<sub>x</sub> burner (Low NO<sub>x</sub> Burner/Package Boiler Simulator). Details regarding the specific designs of these systems have been presented elsewhere [Snow and Lorrain, 1987; Pershing et al., 1973; Mulholland and Srivastava, 1988].

Although several analytical techniques in addition to gas chromatography with electron capture detection (GC/ECD) are applicable to on-line N2O analysis from combustion sources [Lanier and Robinson, 1986; Roby and Bowman, 1987; Muzio et al., 1989; Montgomery et al., 1989], most involve extractive sampling. The sampling system used at this laboratory included extractive sampling through a stainless steel sampling probe, 0.64 cm (0.25 in.) outside diameter (O.D.) heated Teflon tubing and heated filter, water removal by use of a refrigeration drying system, and then pumping by means of a Teflon diaphragm sample pump through calcium sulfate (CaSO<sub>4</sub>) desiceant to continuous emission monitors (CEMs). CEMs included measurement of O2, CO, CO2, SO2, and NO. Immediately after the sample pump, but before desiccation, a portion of the sample was directed to a 1 ml/six port GC sampling valve for on-line N2O analysis by GC/ECD (Shimadzu Model GC-9A). SO2 was measured from a heated sample taken downstream of the filter and upstream of the refrigeration dryer. The GC used to quantify N2O utilized 5 percent methane in argon carrier gas at a flow rate of 20 ml/min., a 3.8 cm (1.5 in.) long by 0.64 cm (0.25 in.) O.D. P<sub>2</sub>O<sub>5</sub> precolumn, a 3.66 m (12 ft) long by 0.32 cm (0.125 in.) O.D. stainless steel Poropak Super Q column (100/120 mesh) at 35°C, and a Ni<sup>63</sup> ECD maintained at 330°C.

Even though this configuration produced N<sub>2</sub>O peaks distinctly separated from CO<sub>2</sub>, considerable effort was made to characterize possible interferences due to co-elution. Tests were conducted with a multicomponent gas standard using the Poropak Super Q column where CO<sub>2</sub> elutes before N<sub>2</sub>O and a molecular sieve 5A column where CO<sub>2</sub> elutes after N<sub>2</sub>O. Comparison of the N<sub>2</sub>O concentrations measured showed no significant differences.

To account for the non-linear properties of the ECD, multipoint calibrations were performed with N2O standards ranging in concentration from 0.24 to 200 ppm. calibration gases used nitrogen as the balance constituent. No column backflushing was employed and no column memory or sensitivity problems were observed during the sub-scale experiments. Laboratory conditions allowed the time to achieve very stable ECD operation, limited the number of analyses per day, and permitted sufficient column conditioning. Laboratory analyses were consistently capable of detecting ambient N2O concentrations with minimum detection limits of 0.24 ppm (based on minimum calibration gas concentration). Method accuracy, expressed as percent deviation, was within 15 percent. Method precision, expressed as percent relative standard deviation, was within 10 percent. N2O standards sent through the sampling system compared with those sent directly through the sampling loop, demonstrating insignificant sampling system bias.

In contrast to the laboratory measurements, column memory and sensitivity problems were observed during the field tests. Memory problems were overcome through the use of multiple instruments. While one system was being used for data collection, others were undergoing column conditioning. Due to the time constraints of field testing, and the necessity to relocate the instrumentation to a new site every several days, some instrument sensitivity was sacrificed. Sufficient time was not allowed to achieve extremely stable baseline ECD operation. However, this loss of sensitivity was deemed acceptable because the scope of these tests were to determine the relative magnitude of direct N2O emissions from full-scale units compared to both the sub-scale experiments and historical data. Field detection limits were consistently below 5 ppm with two tests below 1 ppm. Accuracy and precision were the same as for the sub-scale tests.

Table 1 presents the combustion conditions and average online N2O and CEM data for 13 EPA tests involving the three combustion units and seven fuels including four types of coal. All samples were taken from stack locations. Data in Table I indicate that the direct N2O emissions from all tests never exceeded 5 ppm. The coal tests showed the highest levels (2 to 4 ppm), with several natural gas and No. 2 fuel oil data sets indicating N2O concentrations less than 0.24 ppm. Little difference could be discerned between the two fuel oil and natural gas tests. Data from the Low NOx Burner/Package Boiler Simulator, with and without air staging for NOx control, showed that, while significant NO reduction was seen with air staging, no measureable effect was detected in N2O concentrations. These N2O data, however, are too close to the instrument detection limit for accurate comparison. The other CEM measurements are similar to those typical of full-scale units. Sulfur contents of the four coals examined ranged from 0.97 to 2.95 weight percent as received.

Independent experimental work on N<sub>2</sub>O emissions from laboratory-scale coal combustors has also been completed at the University of Arizona (UA) under the sponsorship of the U.S. Department of Energy (DOE). The downfired laboratory combustor used in that work was very similar in size and design to that described above for the EPA tests, except that the pulverized coal flame was "premixed," and the overall configuration resembled a plug flow reactor. Sampling and analysis for N<sub>2</sub>O was also developed and tested independently. Here the flue gas sample to be analyzed was withdrawn through

TABLE 1. Average On-Line Concentrations Taken From Laboratory and Pilot-Scale Combustion Systems

Unit	Fucl	SR <sup>a</sup>	N <sub>2</sub> O, ppm	NO, ppm	SO <sub>2</sub> , ppm	СО, ррт	02,%	∞2,%	
DF Tunnel Fumace <sup>b</sup>	Utah bit, coal	1.42	4.2	757	753	17	5.5	13.9	
	Montana sub-bit, cosl	1.43	2.2	613	380	30	5.3	14.6	
	W. Kentucky bit, coal	1.46	3.7	553	1650	12	6.8	12.6	
	Pittsburgh bit, coal	1.33	2.2	570	1450	,c	5.7	12.9	
NA Boiler <sup>d</sup>	Natural gas	1.24	< 0.24	62	0	0	4.4	8.9	
	#2 Fuel oil	1.25	0.30	105	58	3	4.4	12.3	
	#5 Fuel oil	1.25	1.3	189	236	16	4.4	14.1	
LNB/PBS <sup>c</sup>	Natural gas	0.73/1.25	< 0.24	50	6	11	4.6	9.2	
	Natural gas	1.10/1.25	0.72	638	4	14	4.6	8.7	
	#2 Fucl oil	0.65/1.26	< 0.24	64	130	2	6.1	12.0	
	#2 Fuel oil	1.13/1.26	0.27	536	130	2	6.0	12.0	
	#5 Fuel oil	0.66/1.29	0.26	60	270	25	5.4	12.2	
	#5 Fuel oil	1.10/1.18	0.73	682	270	25	4.1	11.0	
UA Coal Furnace <sup>f</sup>	Utah bit. coal	1.25	1.28	1121	•	-	4.25	14.0	
	Utah bit. coal	0.65/1.08	1.99	605	•	-	3.60	14.3	
	Utah bit, coal	0.86/1.08	3.80	216	-	-	3.50	14.8	
	Utah bit. coal	1.10/0.90/1.06	4.45	382	-	-	3.85	13.8	

Concentrations presented as measured, dry (SO2 wet) no correction to constant percent O2.

Low NO, Burner/Package Boiler Simulator.

a water-cooled, water-quenched probe. The water was removed in a refrigerated knockout pot, and N2O analysis was by GC/ECD. The latter consisted of a 1 ml sampling loop, a 3.66 m (12 ft) long by 0.32 cm (0.125 in.) O.D. Poropak Q column in stainless steel, at 35°C, and 20 ml/min. of argon/5.22 percent methane carrier gas. The column was periodically reconditioned at a temperature of 220°C. The detector temperature of 250°C led to somewhat decreased sensitivity towards N2O but was chosen to extend the life of the ECD in the presence of oxygen in the flue gas. The detection limit for N2O was 0.1 ppm, but the response was not linear over the entire 0 to 95 ppm range. Precision was within 2 percent of the mean. There was excellent separation between CO2 and N2O, and no measurable interferences by CO2, water vapor, or oxygen. Calibrations were conducted before and after each test run. Backflushing of the column was not found to be necessary, although here the time interval between two samples was about 1.5 hours. In general, the calibration held to within 3 percent of the reference standards over five days of testing, and column memory effects were not noticed.

Figure 2a shows values of exhaust NO and  $N_2O$  emissions as a function of stoichiometric ratio for a Utah bituminous coal.  $N_2O$  levels in Figure 2a vary from 0.5 to 1.5 ppm. Residence time resolved profiles during air staging are shown on Figures 2b (primary SR=0.86) and 2c (primary SR=0.65), and demonstrate the interesting fact that staging causes an increase in  $N_2O$  near the staging point. However,  $N_2O$  levels are still exceedingly low and so the effect is not of practical significance. Air staging is a combustion modification used for  $NO_x$  control whereby a portion of the air necessary for combustion is diverted to a location downstream of the primary flame. This configuration produces an initial fuel rich zone which promotes fuel nitrogen conversion to  $N_2$ . The remaining air is then added to complete the combustion

process. Figure 2d shows residence time resolved NO and  $N_2O$  profiles along the combustor axis while using reburning as a  $NO_x$  control technique. Reburning (or fuel staging) is another combustion modification used for  $NO_x$  control whereby portions of both fuel and air are diverted to locations downstream of the primary flame. Under this configuration, three zones of different stoichiometry are established and adjusted to minimize  $NO_x$  formation. We observed an increase of  $N_2O$  at the point of air injection, similar to that observed under air staged conditions. For all configurations, however, these on-line measurements of  $N_2O$  yielded extremely low values, and indicated that direct  $N_2O$  emissions (from pulverized coal combustion) did not appear to be large, either with or without combustion modifications for  $NO_x$  control.

### Field Tests

Following the laboratory and pilot-scale experiments, EPA sponsored a field study to characterize the direct emissions of NoO from full-scale, pulverized-coal-fired utility boilers. These measurements were conducted at six boilers ranging in size from 165 to 700 MW, including Circular, Triple Cell, and Tangential designs manufactured by Babcock & Wilcox, Riley Stoker, and Combustion Engineering. These units represent a cross-section of the types of boilers currently, and historically since 1950, in use in the U.S., and burned primarily a medium sulfur Alabama bituminous coal, with a reported sulfur content between 1.5 to 2.0 percent. The sampling and analytical methods used were similar to those described above for the EPA sub-scale experiments. Table 2 presents the average on-line NoO and CEM data for each of the six utility units. All on-line N2O measurements were below 5 ppm. In fact, almost all of the on-line N2O measurements were below the detection limits of the GC/ECD systems used for these field tests. These samples

Stoichiometric ratio.

b Downfired Tunnel Furnace.

<sup>&</sup>lt;sup>c</sup> Missing data.

d North American Boiler.

University of Arizona Coal Furnace (corrected to 0 percent O2 dry).

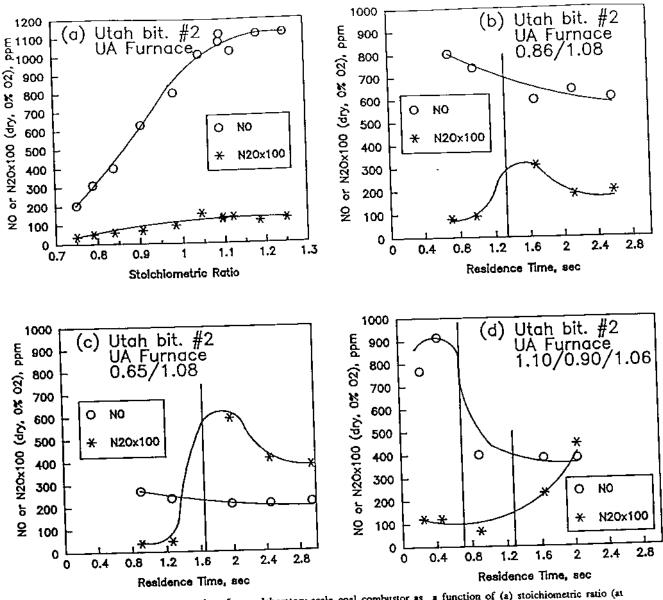


Fig. 2. NO and N<sub>2</sub>O concentrations from a laboratory-scale coal combustor as a function of (a) stoichiometric ratio (at combustor exhaust), and residence time using air staging (b) SR=0.86/1.08, (c) SR=0.65/1.08, and natural gas reburning (d) SR=1.10/0.90/1.06 strategies for NO<sub>X</sub> control.

were taken at existing sampling locations, downstream of all economizer and particulate removal equipment, either before or after the systems' induced draft fans. All six units were operated at or near full load during the tests. Limited SO<sub>2</sub> data were collected due to problems with the SO<sub>2</sub> analyzer.

A summary of the on-line data from both the sub-scale and full-scale studies is presented in Figure 3. Again, these data (indicated by the shaded symbols) are compared to the data base presented by Hao et al. [1987] (open symbols). These results suggest that the direct emission of N<sub>2</sub>O from pulverized-coal-fired utility boilers is very low (less than 5 ppm), that the existing data are suspect due to a sampling artifact [Muzio et al., 1989], and that no simple N<sub>2</sub>O/NO<sub>x</sub> correlation exists. In order to build a stronger case supporting the new on-line measurements against the previous sample container derived data, it was necessary to explore, in more detail, the sampling artifact that may have distorted the historical data base shown on Figure 1.

## TIME RESOLVED N2O MEASUREMENTS FROM SAMPLE CONTAINERS

Concurrent with all on-line activities, extracted samples were collected in stainless steel sampling containers for time dependent analyses of N<sub>2</sub>O by GC/ECD, NO by GC/thermal conductivity detector (TCD), and SO<sub>2</sub> by GC/flame photometric detector (FPD) techniques. These samples were collected at three degrees of dryness including wet samples (before refrigeration drier), partially dried samples (immediately after refrigeration drier), and desiccated samples (after additional drying by use of a P<sub>2</sub>O<sub>5</sub> filled canister). Samples from the subscale experiments were analyzed after 1, 4, 24, 48, 168, and 336 hours. Samples from the full-scale tests were analyzed after 1, 4, 48, 168, and 336 hours.

Samples for time resolved analyses were collected in 0.5 L stainless steel (304) containers. These containers were fitted with stainless steel needle valves at each end and one septum

TABLE 2. Average On-Line Concentrations Taken From Full-Scale Utility Boilers

Unit	Sizc, MW	Class/Type <sup>8</sup>	Manufacturer	N <sub>2</sub> O, ppm	NO, ppm	SO <sub>2</sub> , ppm	СО, ррп	02.%	CO <sub>2</sub> , %
A B C D	250 250 250 165 700 165	Pre-NSPS/Circular Pre-NSPS/Triple Cell Pre-NSPS/Circular Pre-NSPS/Tangential Pre-NSPS/Tangential Pre-NSPS/Tangential	Babcock & Wilcox Babcock & Wilcox Riley Stoker Combustion Engineering Combustion Engineering	1.3 <3.6 <3.6 <1.2 0.7 <1.2	386 513 559 354 374 319	_6 - - - - 930	13.3 8.6 2.2 30.7° 3.1	4.6 7.1 6.1 8.3 6.0 8.1	14.8 13.5 14.3 11.7 13.1 11.9

Concentrations presented as measured, dry (SO<sub>2</sub> wet), no correction to constant percent O<sub>2</sub>.

fitting for sample extraction by gas syringe. Since we realized that much of the historical data was based on glass containers, a number of samples were collected in glass containers of similar size for comparison. While the available data for this comparison are limited, the behavior of the sample in the glass containers was similar to that in the stainless steel containers, except as noted below. The stainless steel containers were rinsed with de-ionized water and dried overnight at 107°C (225°F). After cooling, each container was fitted with a septum and then leak tested to 40 mm Hg. Following the leak check, the valves were closed and ends capped. The container interiors were not polished or treated with any coating. Combustion gas and N2O calibration gas (10 ppm) samples of varying moisture content were passed through beds of different desiccants and analyzed to determine any effect of selective water removal on N2O. Three desiccants were tested including phosphorus pentoxide (P2O5), magnesium perchlorate [Mg(ClO<sub>4</sub>)<sub>2</sub>], and silica gel (SiO<sub>2</sub>). None of these desiccants was seen to affect the N2O concentration. P2O5 was chosen as the desiccant of choice for these tests due to its greatest quantitative ability to remove water.

Figure 4 presents results of these time resolved analyses from sample containers containing effluent from selected laboratory and full-scale tests. Figure 4a (laboratory combustor) shows that N2O is rapidly formed from an initial value of 4.2 ppm to a level approaching 200 ppm, when condensed water was present, to half that value when water was physically removed by a refrigerated knockout pot and to less than 30 ppm when the sample was desiccated. Data from glass containers showed similar asymptotes in N2O, but a slower rate of increase at early analysis times. This observation is illustrated by comparing the N2O concentrations as they evolve in the two container materials of samples taken from experiments burning a western Kentucky coal. In stainless steel, the refrigerated dried sample evolves from 3.7 ppm (online) to > 50 ppm within 4 hours. In glass, the evolution after 4 hours for a similar sample is only 24 ppm. In fact, concentrations approaching 50 ppm were not measured in the glass container until the analysis at 168 hours. Figure 4b shows that the rise of N2O is accompanied by a drop in gaseous SO2 in the sample container, indicating the importance of sulfur as well as of moisture, in this low temperature mechanism. Figure 4c presents similar N2O evolution data for

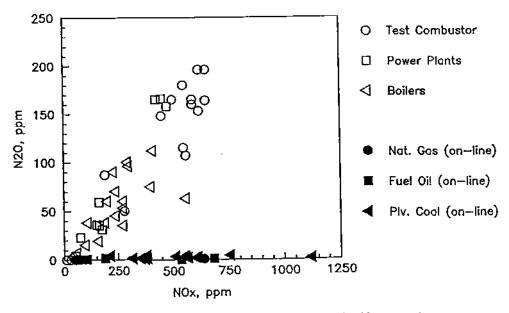


Fig. 3. Historical N<sub>2</sub>O data base as presented in Figure I, compared to on-line data taken by this group. Open symbols represent the data presented by *Hao et al.* [1987]. Shaded symbols represent data taken by this group from full- and sub-scale combustion systems burning several types of coals, fuel oils, and natural gas using an on-line GC/ECD sampling/ analysis technique.

<sup>&</sup>lt;sup>2</sup> All units burned a medium sulfur Alabama bituminous coal.

b Missing data.

CO trace showed numerous spikes.

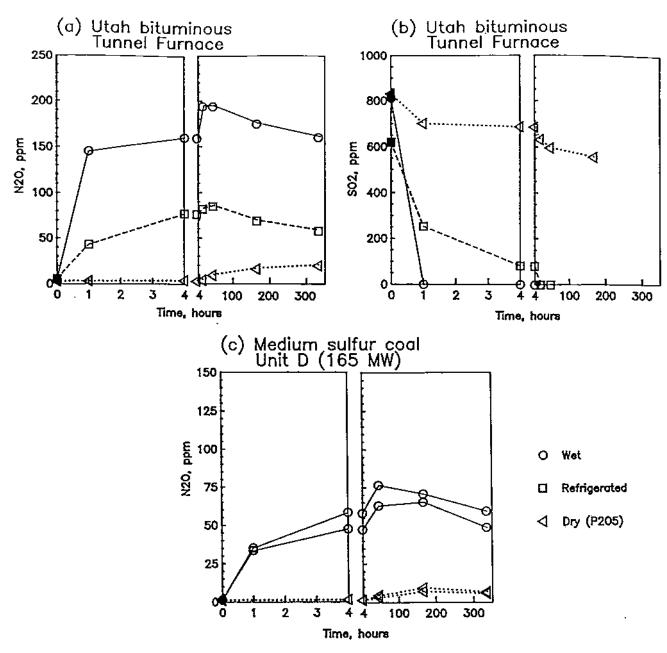


Fig. 4. Evolution of N2O and SO2 (vapor phase) with time from coal combustion samples collected and stored in stainless steel sampling containers at three degrees of sample dryness. Stack emission samples were collected using the (a, b) Downfired Tunnel Furnace burning Utah bituminous coal (SR=1.42), NO(initial)=757 ppm, and (c) Unit D (full-scale utility boiler) burning medium sulfur Alabama bituminous coal, NO(initial)=354 ppm.

the full-scale coal-fired utility boiler tests from unit D. It is interesting to note that both the sub-scale and full-scale N2O data from wet or partially dry samples show rapid increases in the first minutes and hours after sampling. The rate of production of N2O was less in glass sample containers, although asymptotic levels, after long times, were similar. Smaller (but non-negligible) increases are seen in the dry samples. Maximum N2O values from wet samples are seen after 24 hours. These values (200 and 75 ppm) are comparable to those presented by the historical data and the proposed N2O-N:NO<sub>x</sub> correlation (Figure 1). The maximum N<sub>2</sub>O concentration is likely related to the initial NO and SO<sub>2</sub> concentrations. This speculation is supported by comparing the N2O and initial NO and SO2 data from these two tests (Tables 1 and 2). Figure 4b shows that the disappearance of SO<sub>2</sub> seems to be very much dependent on the sample dryness. NO data (not presented) all show rapid removal/reaction (possibly forming NO<sub>2</sub>) within 1 to 4 hours regardless of the moisture content of the samples. These results are consistent with the recent data of *Muzio and Kramlich* [1988] and *de Soete* [1988, 1989a, 1989b].

Similar data trends were obtained for No. 5 and No. 2 fuel oils burned in a standard firetube package boiler and a special research combustor designed to test NO<sub>x</sub> abatement techniques. While the trends are similar to those seen for coal, the magnitude of the artifact is much less for the two fuel oils. These data are also consistent with the supposition that the resulting N<sub>2</sub>O formation is dependent on the initial NO and SO<sub>2</sub> levels (in addition to the moisture). The N<sub>2</sub>O increases seen in the Package Boiler Simulator samples (where NO<sub>x</sub> control was

used) are significantly smaller than those seen in the North American Boiler samples (without NO<sub>x</sub> control) burning the same fuels. Tests on natural gas combustion effluents indicated a measurable, albeit smaller, effect even though SO<sub>2</sub> values were below detectible (for our instrumentation) levels.

Figure 5 summarizes all the time resolved data and shows how the maximum yield of N<sub>2</sub>O formed in the sample container (after approximately 48 hours) depends on the initial NO in the flue gas. We believe that the similarity with the historical data base shown in Figure 1 is not coincidental and that the previously accepted N<sub>2</sub>O/NO<sub>x</sub> emission ratio can be explained on the basis of this sample container artifact. The true N<sub>2</sub>O emission levels, shown as shaded symbols, are independent of the initial NO and never exceed 5 ppm for combustion units tested.

### CONCLUSIONS

The new N<sub>2</sub>O emission data base from both field and laboratory combustion units indicated that direct N<sub>2</sub>O emissions from conventional fossil fuel combustion units were very low, and would lead to a global N<sub>2</sub>O flux that is lower by a factor of 50 to 100 than that inferred from previous work and that could account for less than 3 percent of the entire anthropogenic N<sub>2</sub>O flux (less than the contribution from fertilizers [Hao et al., 1987]). This has strong implications regarding the need, or lack of need, to control N<sub>2</sub>O emissions from these combustion sources. Furthermore, in contrast to previous suggestions, our laboratory combustor data indicate that the most promising combustion modifications for NO<sub>x</sub> control might actually lead to a small increase in N<sub>2</sub>O emitted, although the net amount is still insignificant.

Discrepancies between these and previous data can be explained by a sampling artifact in which N<sub>2</sub>O is produced from NO in the presence of SO<sub>2</sub> and water in sample containers. This artifact, which occurs at room temperatures, can easily lead to the erroneous conclusion (used in previous estimates of the global N<sub>2</sub>O flux) that N<sub>2</sub>O directly emitted from combustion equipment is significant and proportional to the NO emitted

Our results do not extend to emerging coal combustion technologies, such as fluidized bed combustion, where significant emissions of N<sub>2</sub>O (>100 ppm) have been observed by researchers who were aware of the sampling artifact [Amand and Andersson, 1989]. However, emerging technologies cannot explain the historical parallelism between the use of coal, the rise in global CO<sub>2</sub>, and the rise in global N<sub>2</sub>O [Weiss and Craig, 1976]. This apparent N<sub>2</sub>O/CO<sub>2</sub> correlation, however, may be simply a circumstantial relationship between increased industrialization and other (non-combustion) anthropogenic sources of N<sub>2</sub>O.

We now know that N<sub>2</sub>O can be produced quickly in sample containers at low SO<sub>2</sub> levels, and at low moisture levels. Even though previous research [Martin et al., 1981], examining reactions of NO<sub>x</sub> with SO<sub>2</sub> in aqueous aerosols, concluded that the rate of N<sub>2</sub>O production seemed too small to significantly change ambient concentrations, it would be most unwise to rule out coal combustion as an indirect source of global N<sub>2</sub>O. Additional research should be completed to eliminate any connection between the emission of acid rain precursors (NO and SO<sub>2</sub>) and global N<sub>2</sub>O production in the atmosphere or local N<sub>2</sub>O production in a power plant exhaust plume. Only then can the impact of fossil fuel combustion on global N<sub>2</sub>O levels be unambiguously delineated.

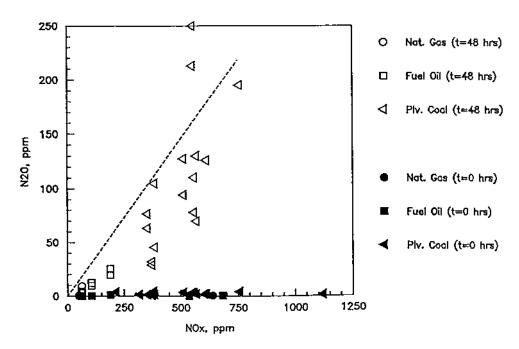


Fig. 5. Comparison of on-line NO emissions to N2O concentrations from on-line (t=0 hours) and aged (t=48 hours) samples. Shaded symbols represent on-line data as presented in Figure 3. Open symbols represent corresponding wet samples that have been allowed to evolve in stainless steel sampling containers for 48 hours. The dashed line represents a proposed N2O-N:NO<sub>X</sub> molar ratio of 0.58:1 [Hao et al., 1987].

Acknowledgments. Portions of this work were conducted under EPA contracts 68-02-4701 and 68-02-4285 with Acurex Corporation, DOE contract DEAC22-87PC78850 with the University of Arizona, and EPA Purchase Order 8D1713NATA with J. O. L. Wendt. The authors would like to thank EPA/AEERU's R. A. Grote for his assistance developing the N2O GC/ECD system. The authors would also like to thank the Acurex field team (R. K. Clayton, K. A. Krebs, R. M. Machilek, and A. Sykes) for their efforts and quick response to the field test schedule. Grateful acknowledgment is made to S. M. Wilson of Southern Company Services and D. M. Burden of Alabama Power Company for arranging the testing of the full-scale boilers. Finally, the authors would like to acknowledge EPA's OPPE and OAR for partial project funding. The research described in this article has been reviewed by the Air and Energy Engineering Research Laboratory, U.S. Environmental Protection Agency, and approved for publication. The contents of this article should not be construed to represent Agency policy nor does mention of trade names or commercial products constitute endorsement or recommendation for use.

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(Received June 15, 1989; revised November 24, 1989; accepted November 24, 1989.)